

Promoting Effects of Se on the Activity and Selectivity of Rh-ZrO₂ Catalyst for Ethene Hydroformylation

Y. Izumi, K. Asakura, and Y. Iwasawa

Department of Chemistry, Faculty of Science, University of Tokyo, Hongo, Bunkyo-ku, Tokyo 113, Japan

Se-Modified Rh-ZrO₂ catalysts, prepared by treatment of Rh-ZrO₂ with Me₂Se or by a co-impregnation method using SeO₂, exhibit high activities and selectivities for ethene hydroformylation, having an optimum ratio of Se : Rh.

While chalcogens such as S and Se are known to have strong poisoning effects on metal catalysis,¹ Se has been found to act as a good catalyst for liquid phase carbonylations² suggesting that the Se atom can interact with and activate carbon monoxide. We now report Se-promoted Rh-ZrO₂ catalysts which exhibit high activities and selectivities for ethene hydroformylation.

Two types of catalysts, (1) and (2), were prepared as follows. ZrO₂ (surface area 12 m² g⁻¹, Soekawa Co., Ltd.) was impregnated with Rh(NO₃)₃ (Soekawa Co., Ltd.) in aqueous solution, followed by calcination in air at 673 K and reduction with H₂ at 673 K for 1 h. CO was preadsorbed onto the Rh-ZrO₂, reaching full coverage³ at 295 K, and the catalyst was treated with Me₂Se (0.025–0.12 kPa) (Toyo Stauffer Chemical Co.) at 373 K for 30 min. The Se-modified catalyst was further treated with H₂ at 373 K for 30 min to remove weakly physisorbed Me₂Se without reaction with surface Rh atoms. The Se-promoted Rh-ZrO₂ catalyst thus obtained was denoted as catalyst (1). Se-modified catalysts (2) were prepared by co-impregnation of ZrO₂ with Rh(NO₃)₃ and SeO₂ (Tri Chemical Co., Ltd.) in aqueous solution, followed by calcination in air at 673 K and reduction with H₂ at 673 K for 1 h. Rh loadings were fixed at 1 or 3 wt%, the Se content was varied in the range Se : Rh 0.01 to 0.17 by changing the amount of Me₂Se or SeO₂. The Se contents of the catalysts were determined by means of X-ray fluorescence. Very little Se was lost from either catalyst (1) or (2) during the calcination, reduction, and hydroformylation reactions.

Ethene hydroformylation was carried out in the temperature range 393–473 K in a closed circulating system (dead volume 119 cm³) using a dry ice-acetone trap (179 K) to isolate propanal and propanol. The activities for the hydro-

formylation as a function of Se content for catalyst (1) are shown in Figure 1. As the Se : Rh ratio increased, propanol formation was considerably enhanced, reaching a maximum at Se : Rh 0.066, while ethene hydrogenation was suppressed. As a result, the selectivity toward oxo-compounds also changed markedly with increasing Se content, having a maximum at Se : Rh 0.066 as shown in Figure 2. The selectivity was four times that of the unmodified Rh-ZrO₂ catalyst.

Figure 2 shows the selectivities to oxo-products in ethene hydroformylation on catalysts (2) with Rh loadings of 1 and 3 wt% plotted against the Se : Rh ratio. Similarly to catalyst (1), propanol formation was enhanced by Se addition, while ethene hydrogenation and propanal formation were reduced. The selectivity for oxo-compounds was maximised at Se : Rh 0.019 for 1 wt% Rh-ZrO₂ and at Se : Rh 0.032 for 3 wt% Rh-ZrO₂.

The activation energies (*E_a*) for the formation of ethane, propanal, and propanol on 1 wt% Rh-ZrO₂ catalyst were 60, 22, and 30 kJ mol⁻¹, respectively. On Se-modified catalyst (2) (Rh 1 wt%, Se : Rh 0.012), which gave almost maximum hydroformylation selectivity, *E_a*'s were found to be 53, 0.9, and 36 kJ mol⁻¹, respectively. While a decrease in *E_a* for propanal formation was observed, the *E_a* for propanol formation was promoted by Se addition. Temperature programmed desorption (t.p.d.) spectra for catalyst (2) (Rh 1 wt%, Se : Rh 0.01–0.07),⁴ in the presence of H₂ in the temperature range 300–773 K, immediately after ethene hydroformylation at 453 K showed desorbed products pro-

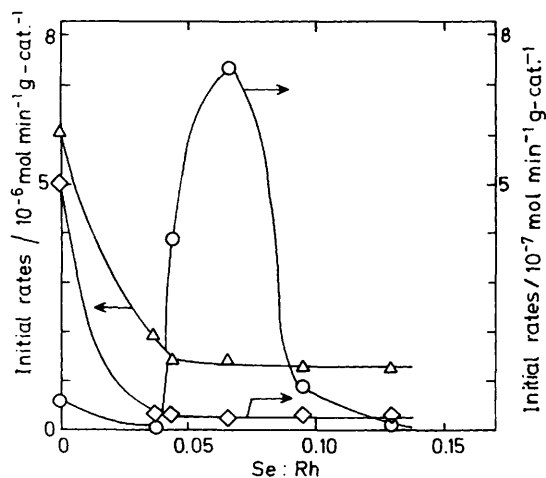


Figure 1. Catalytic activities of Se-modified catalysts (1) for ethene hydroformylation as a function of Se content; reaction temp. 453 K, total pressure 4.0×10^4 Pa; C₂H₄ : CO : H₂ 1 : 1 : 1, Rh-ZrO₂ 1 wt%; Δ ethane, \diamond propanal, \circ propanol. Scales on the left and right vertical axes refer to the formation of ethane and of propanal and propanol, respectively, as indicated by arrows.

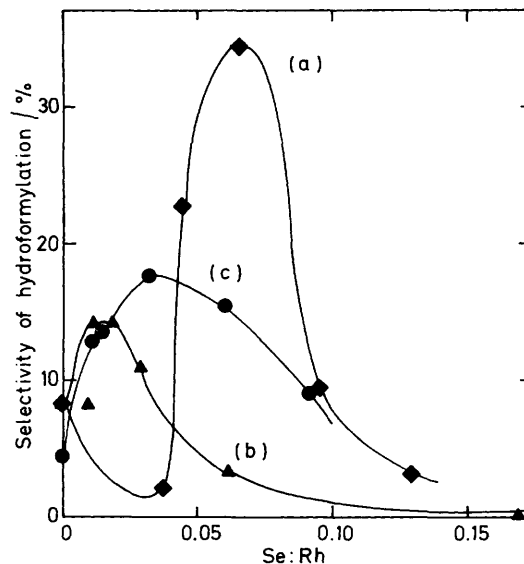


Figure 2. Selectivities of ethene hydroformylation on Se/Rh-ZrO₂ catalysts (1) and (2) as a function of Se content; (a) catalyst (1) (Rh 1 wt%), (b) catalyst (2) (Rh 1 wt%), (c) catalyst (2) (Rh 3 wt%), reaction temp. 453 K; total pressure 4.0×10^4 Pa; C₂H₄ : CO : H₂ 1 : 1 : 1.

panol, ethene, ethane, and CO. The desorption peak temperature and the peak area, which varied with Se:Rh ratio, suggested that intermediate propanoyl species (EtCO) were more stabilized on Se-modified Rh catalysts than on unpromoted Rh/ZrO₂, enabling them to evolve long enough for further hydrogenation to occur to produce propanol. The amount of the intermediate species was markedly reduced on the catalyst modified with more Se.

X-Ray photoelectron spectra (x.p.s.) showed that the binding energy of Se 3d_{5/2} is modified by increasing amounts of Se. It had a value of 53.2 eV for catalyst (1) and 53.1 eV for catalyst (2), indicating that the oxidation state of Se was 2-, independent of Se content in the range of Se:Rh 0.01–0.13, while Rh had 3d peaks corresponding to the metallic state⁵ for both catalysts (1) and (2). H₂ adsorption decreased steadily as Se quantity increased,⁶ eventually to almost zero. However, for CO adsorption the decrease was less marked and the more Se-modified surface still adsorbed CO, suggesting that CO molecules are adsorbed on or around Se–Rh ensembles more easily than H₂.⁷

The marked promoting effects of Se on the activity and selectivity of Rh–ZrO₂ catalysts for ethene hydroformylation may thus be ascribed to the preferable interaction of CO with Se²⁻ on Rh, the resulting promotion of CO insertion to C₂H₅, and the stabilization of intermediate propanoyl species leading to the formation of propanol by Se–Rh ensembles.

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